

Direct Numerical Simulations of Nonpremixed Flame Quenching by Fine Water Droplets

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Diffusion Flame Extinction



□ Extinction Mechanisms:

- **Aerodynamic quenching:** flame weakening due to attenuation of reactivity as a result of reduced flame residence time

$$\chi_{st} \geq \chi_{st,ext}^{ref}$$

- **Thermal quenching:** flame weakening due to heat losses

- Convection/conduction to the walls
- Radiative heat loss
- Dilution (e.g. air vitiation)
- Water evaporation

$$\chi_{st} \geq \underbrace{\chi_{st,ext}}_{\text{critical value}} = \underbrace{\chi_{st,ext}^{ref}}_{\text{critical value at reference conditions}} \times \exp\left(-T_a \left(\frac{1}{T_{st}} - \frac{1}{T_{st,ext}^{ref}}\right)\right)$$

: Wang & Trouvé (2006) *Combustion and Flame*

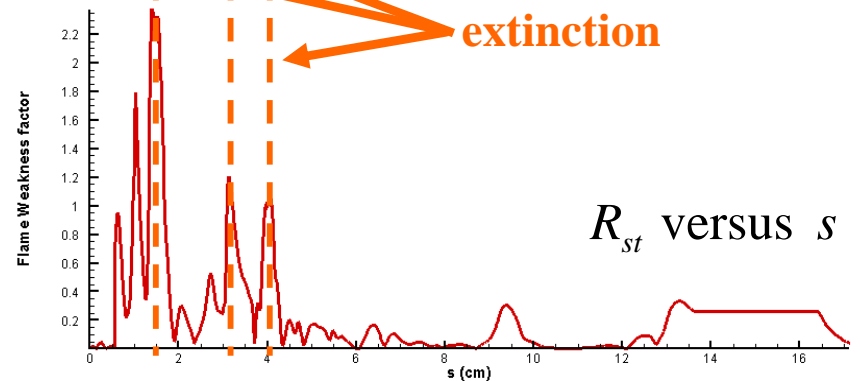
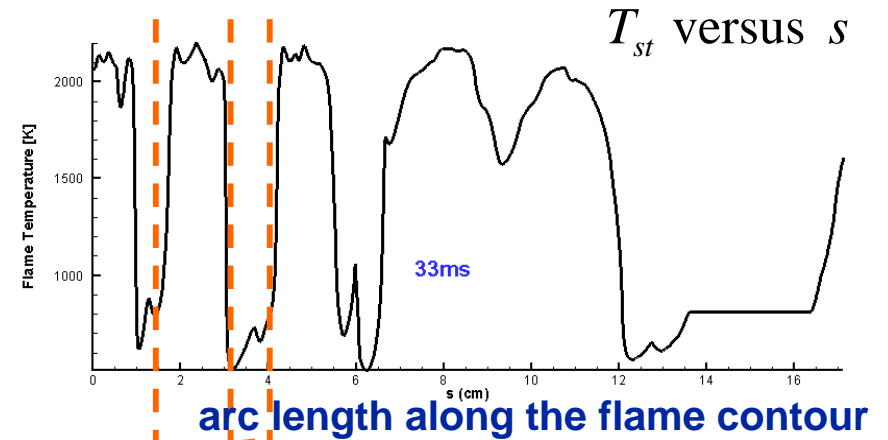
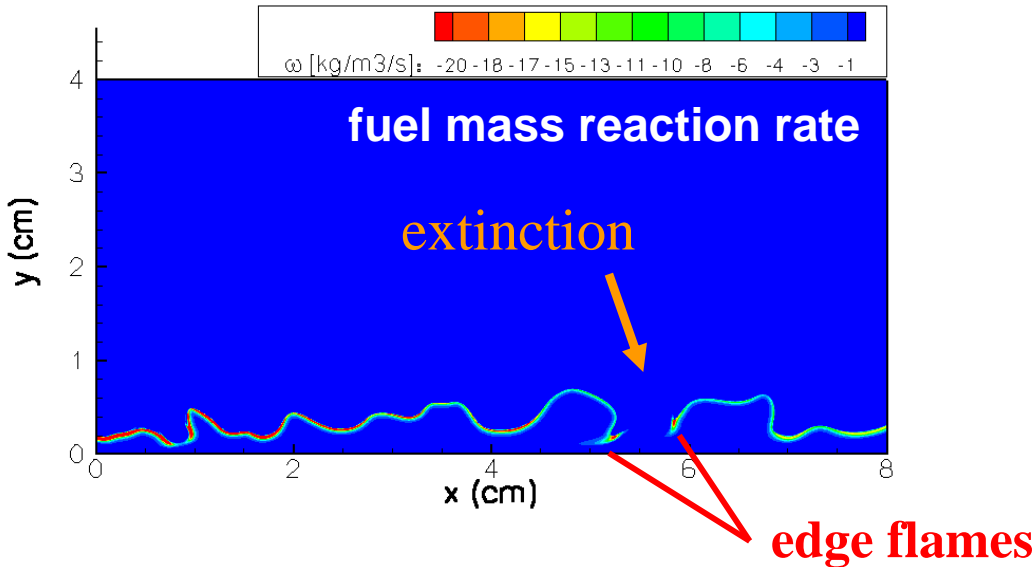
Modified extinction criterion for flame-wall interaction

Flame-Wall Interaction

Narayanan & Trouve (2007) – See also CP11 “Soot and Radiation”



Non-premixed C₂H₄-air turbulent jet diffusion flame near a wall



Extinction criterion

$$R = \frac{\chi_{st}}{\chi_{st,ext}} = \frac{\chi_{st}}{\chi_{st,ext} \exp(\beta H)} \geq 1$$

Flame weakness factor

Wall cooling factor

$$\beta = \frac{T_a (T_{st}^{ad} - T^\infty)}{(T_{st}^{ad})^2} \quad \text{Zeldovich number}$$

$$H = \frac{c_p (T - T^\infty)}{\Delta H_f} \left(\frac{1}{Y_F^\infty} + \frac{1}{(Y_{O_2}^\infty / r_s)} \right) + \frac{Y_F}{Y_F^\infty} + \frac{Y_{O_2}}{Y_{O_2}^\infty} - 1$$

Excess enthalpy (< 0)

Objectives



Laminar/Turbulent Nonpremixed Flame Extinction by Water Spray

DOE INCITE 2007 (U. Michigan, U. Maryland, U. Wisconsin)

(Innovative and Novel Computational Impact on Theory and Experiment)

Science Issues

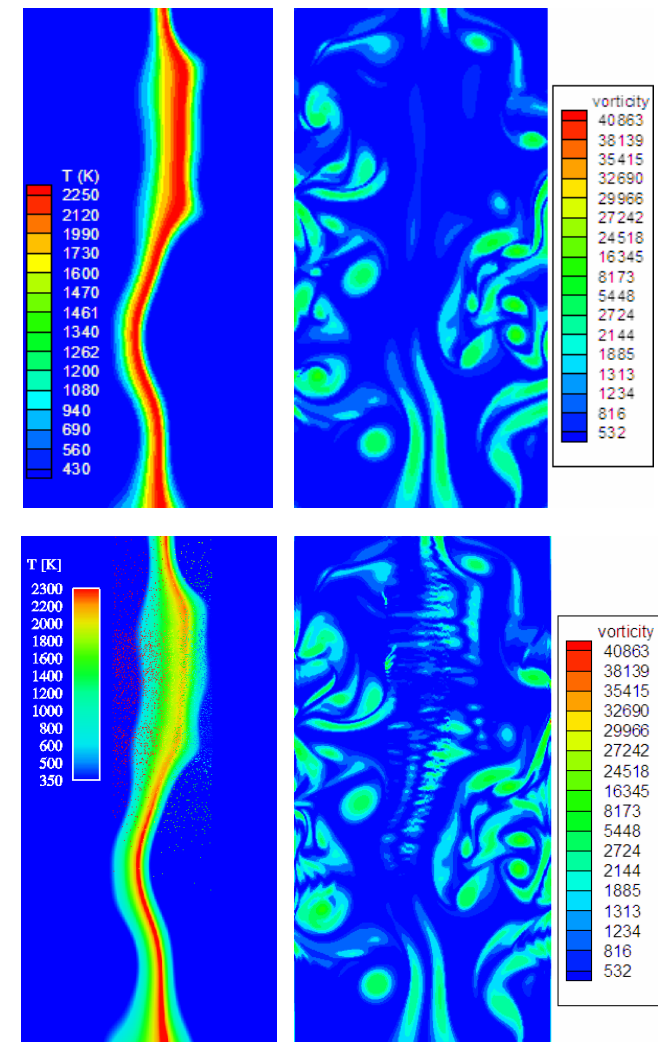
- Extinction by flame cooling due to spray
- Strain- & spray-induced quenching
- *Unified extinction criteria accounting for heat/radical losses due to water spray evaporation*

High-fidelity simulation to demonstrate advanced physical submodels

- Optically thick gas and soot radiation
- Lagrangian spray model
- Improved characteristic boundary conditions

Three-dimensional counterflow simulation (in progress)

- Rectangular Cartesian coordinate
- Domain size $\approx 10\text{cm}^3$, 10 million grid points, physical time $\approx 20\text{ms}$
- $\text{Re} \approx 100$, $\text{Da} \approx 3\text{-}4$, strain rate $\approx 1000\text{s}^{-1}$



Model Configuration



□ 2-D Counterflow Nonpremixed flame

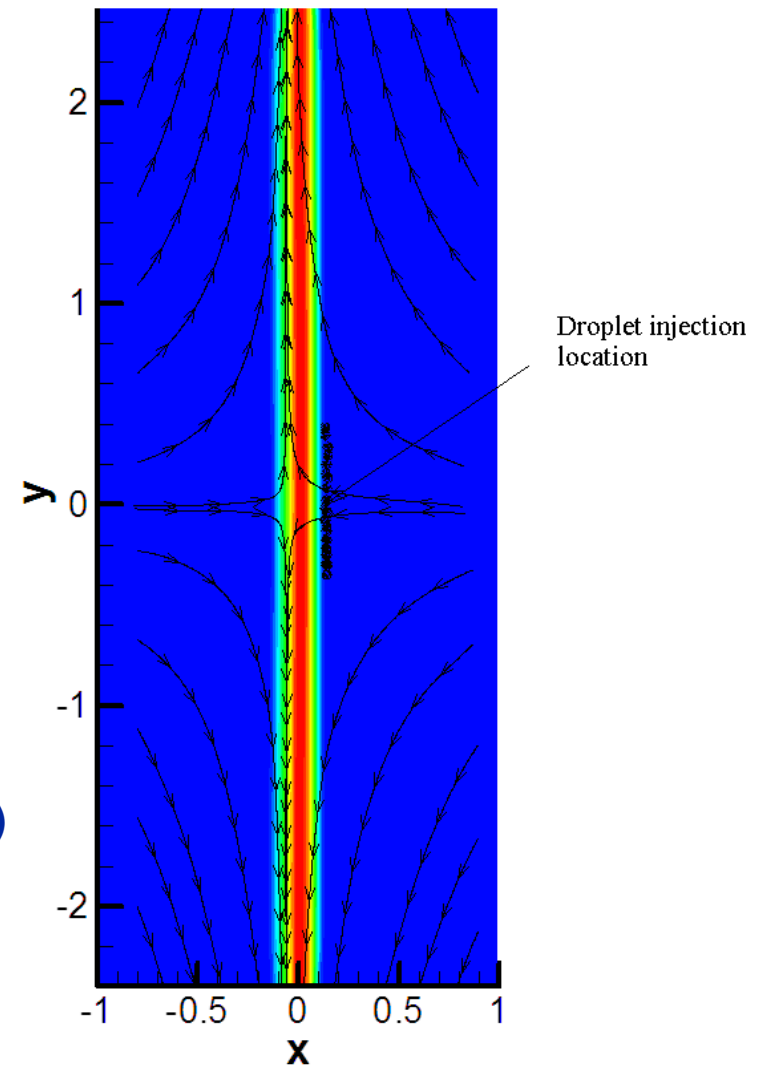
- High-order finite-difference (S3D)
- Modified NSCBC at inflow/outflow boundaries
- Lagrangian spray model (Rutland)
- Ethylene vs. air (DRG mechanism, Lu & Law)
- Gray gas radiation, discrete ordinate method

□ Computational Parameters

- Domain size: 5cmx2cm (800² grid points)
- $\chi_{st} = 20 \text{ s}^{-1} \sim 0.4\chi_{st,ext}$
- Homogeneous turbulence injected at the inlet ($u'/U = 2.0$, $L_{11} = 1.25\text{cm}$)

□ Spray parameters

- Spherical, monodisperse ($d=40 \mu\text{m}$, mist regime)
- Injected 1.4mm from the flame at the local gas velocity
- Loading: 15%/32%/80% of local heat release



Unified Extinction Criterion



Excess enthalpy for multi-component systems

$$H = \frac{\Delta h_{th}(T, Y_k)}{h_F^0 \times Z_{st} + h_O^0 \times (1 - Z_{st}) - \left(\sum_k h_k^0 Y_k^{eq}(Z_{st}) \right)}$$

$$\Delta h_{th}(T, Y_k) = \left(\int_{T_0}^T c_p dT \right) - \left[\left(\int_{T_0}^{T_F} c_{p,F} dT \right) \times Z + \left(\int_{T_0}^{T_O} c_{p,O} dT \right) \times (1 - Z) \right] - \left[h_F^0 \times Z + h_O^0 \times (1 - Z) - h^0 \right]$$

mixing

heat release

$$c_p = \left(\sum_k c_{p,k} Y_k \right) ; c_{p,F} = \left(\sum_k c_{p,k} Y_{k,F} \right) ; c_{p,O} = \left(\sum_k c_{p,k} Y_{k,O} \right)$$

$$h^0 = \left(\sum_k h_k^0 Y_k \right) ; h_F^0 = \left(\sum_k h_k^0 Y_{k,F} \right) ; h_O^0 = \left(\sum_k h_k^0 Y_{k,O} \right)$$

➤ **$H = 0$ accounts for effects of heat loss and differential diffusion**

Extinction Criterion:

$$R = \frac{\chi_{st}}{\chi_{st,ext}} = \frac{\chi_{st}}{\chi_{st,ext}^{ad} \exp(\beta H)} \geq 1$$

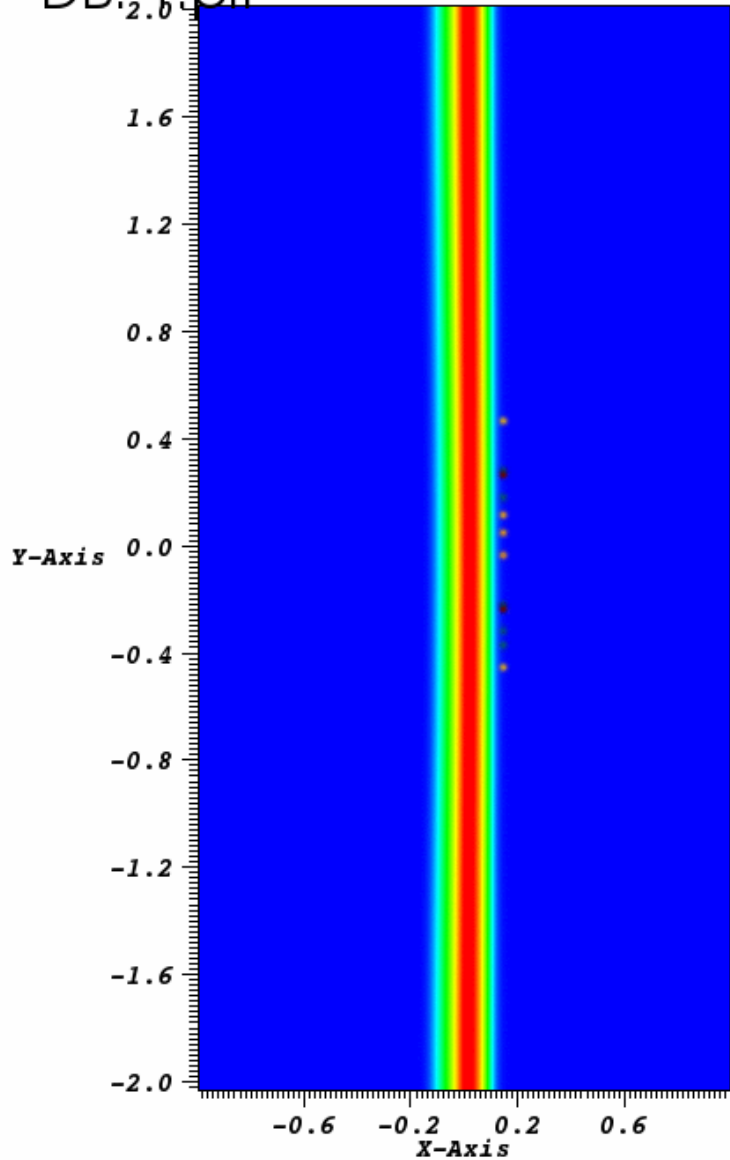
where the Zeldovich number (β) is determined based on Law *et al.*

$$T_a = \frac{E_a}{R^0} = -2 \frac{\partial \ln f^\circ}{\partial (1/T_b^\circ)} \quad (f^\circ = \rho_u S_L)$$

Laminar Flame Results (32% loading)

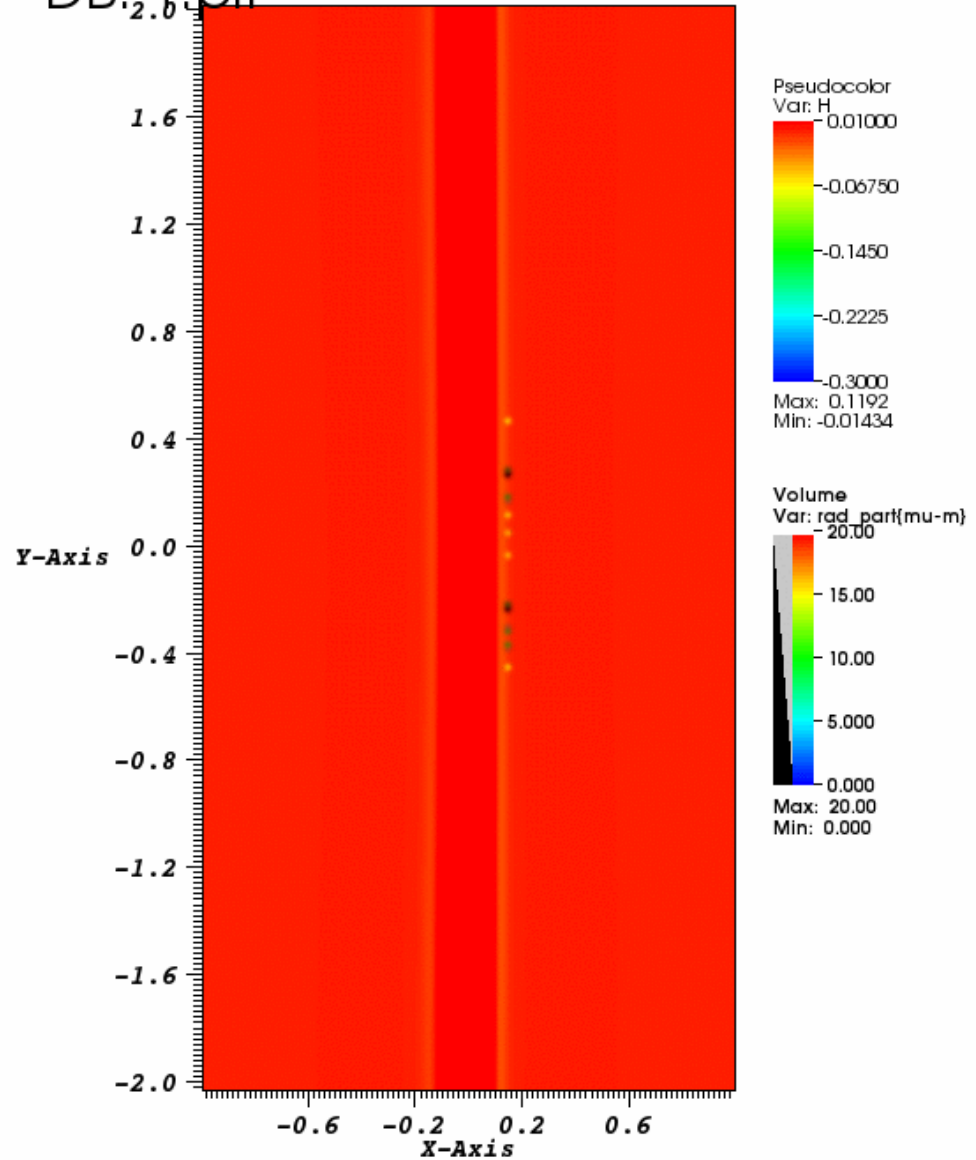


DB:2.1.plt



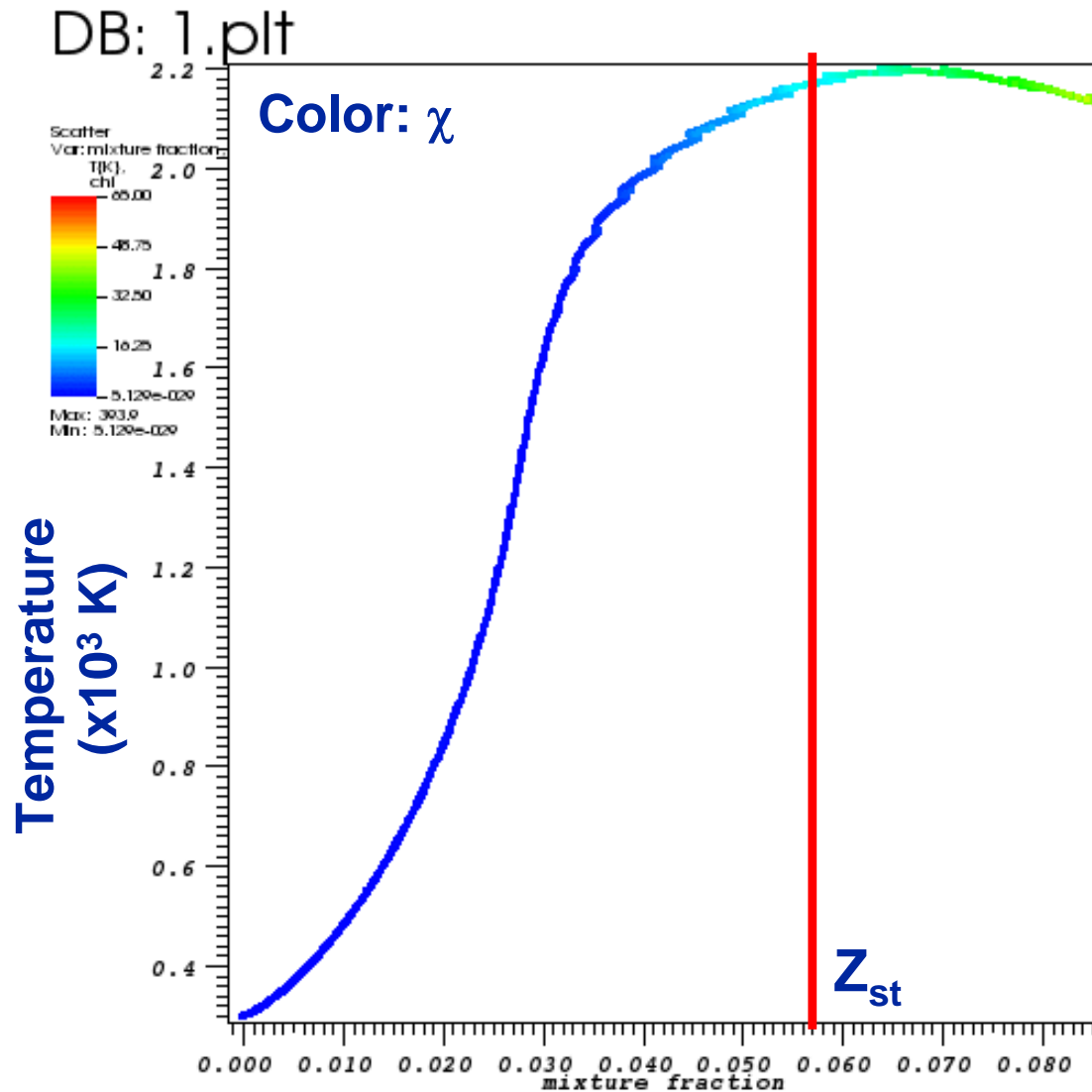
Temperature

DB:2.1.plt

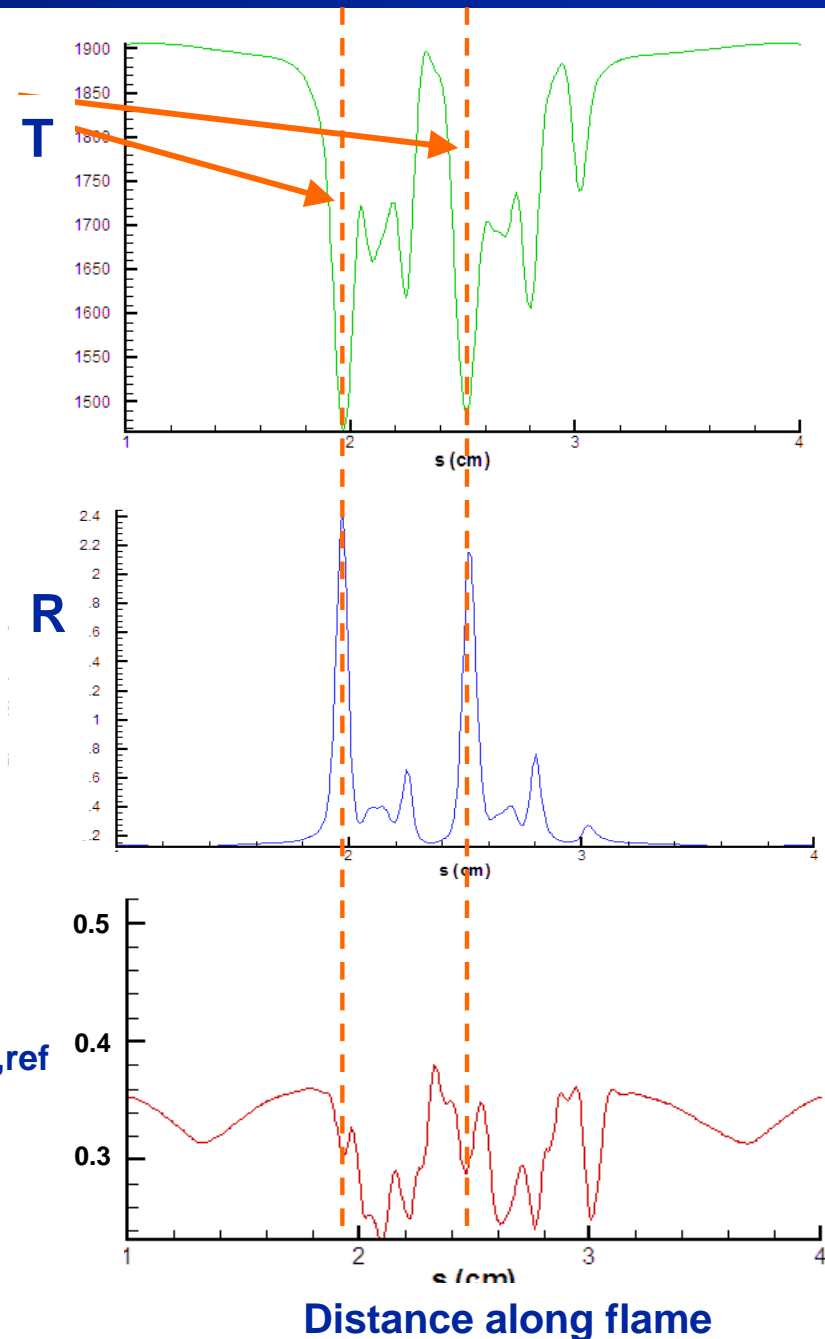
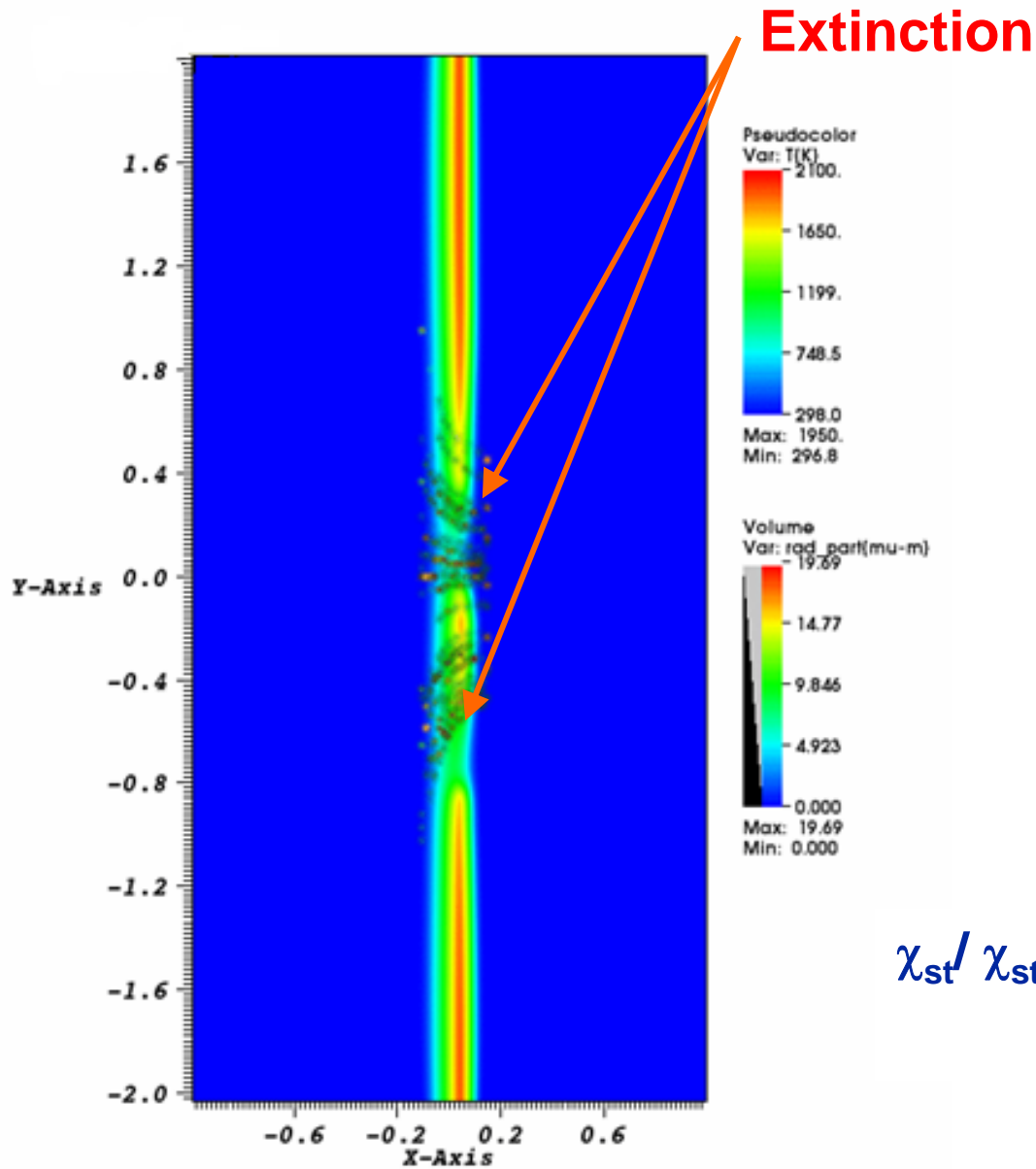


Excess enthalpy variable

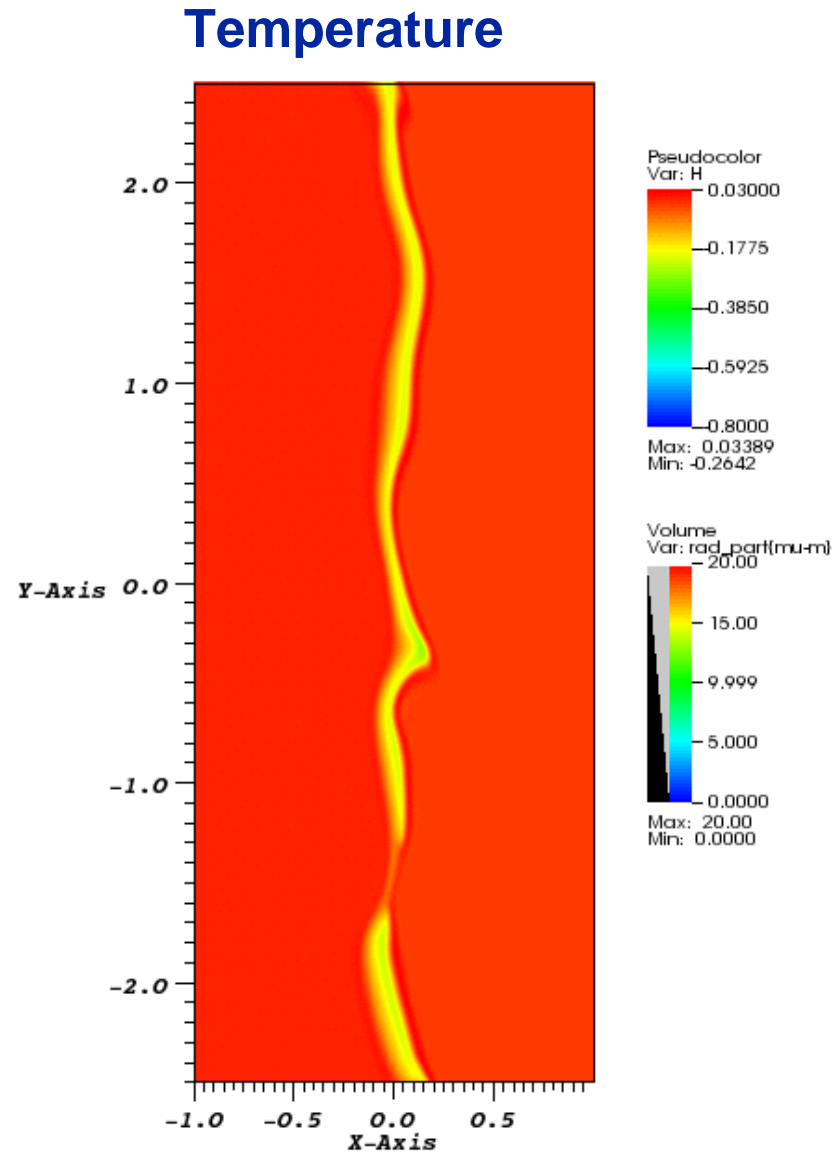
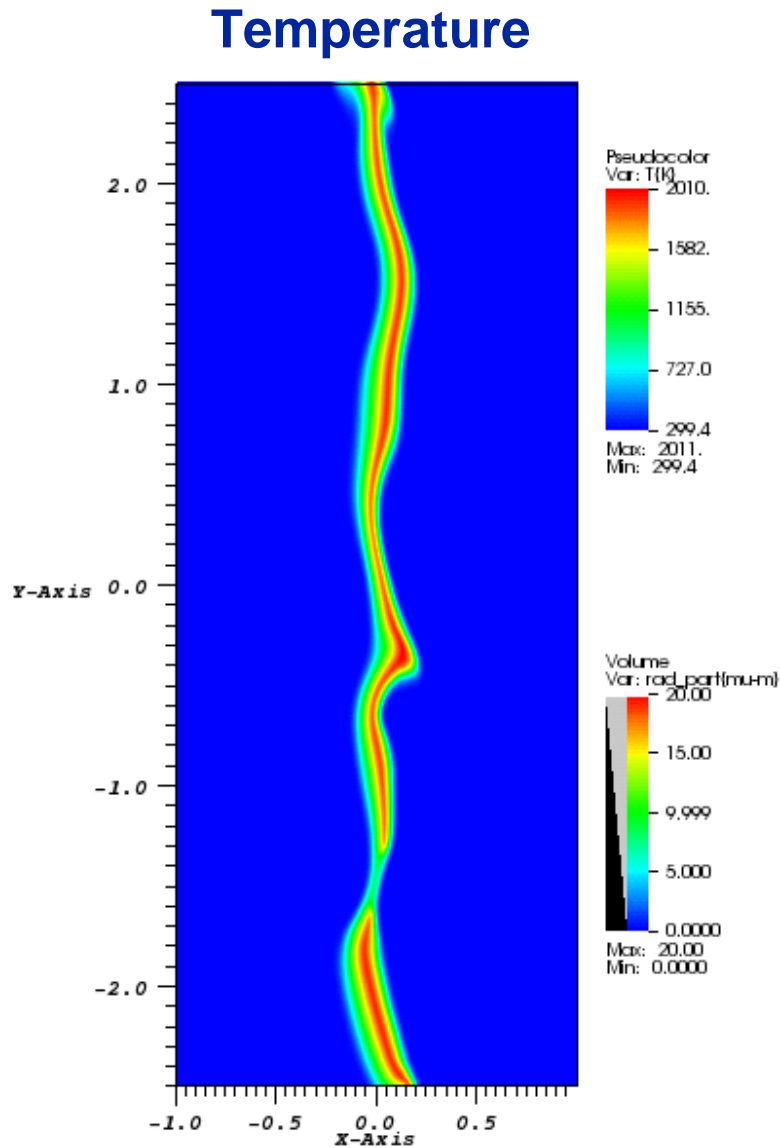
Laminar Flame Results (32% loading)



Extinction Analysis

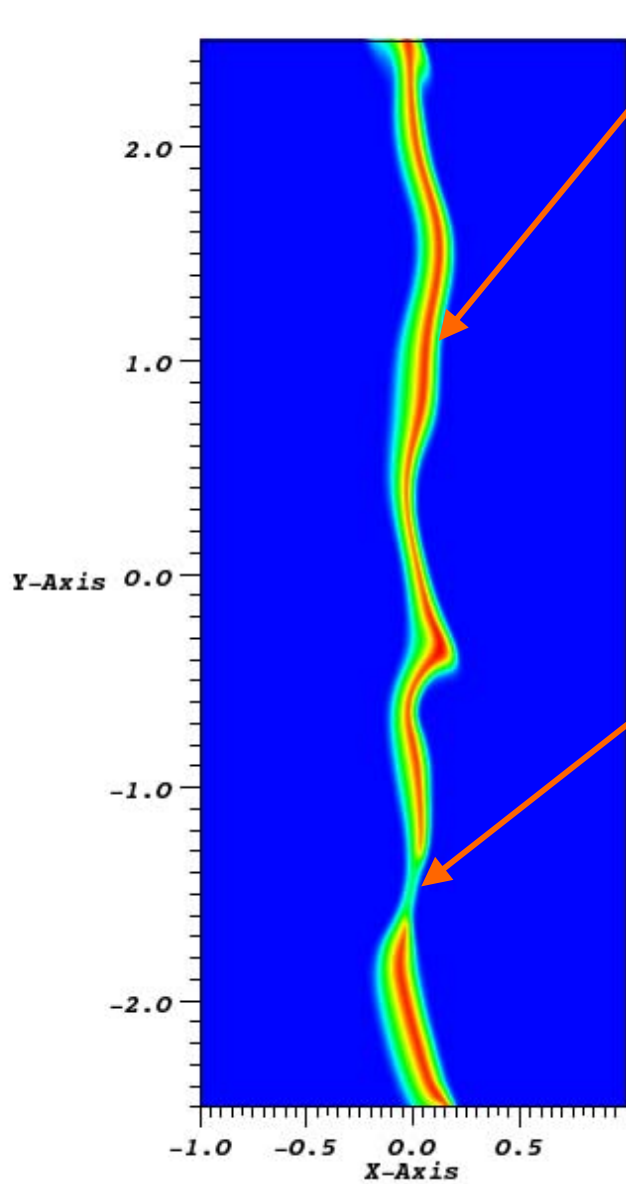


Turbulent Flames with Spray

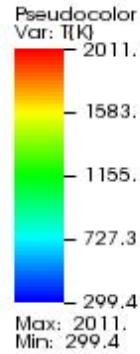


Time duration 2.85ms-4.54ms

Turbulence without spray



Flame strengthens



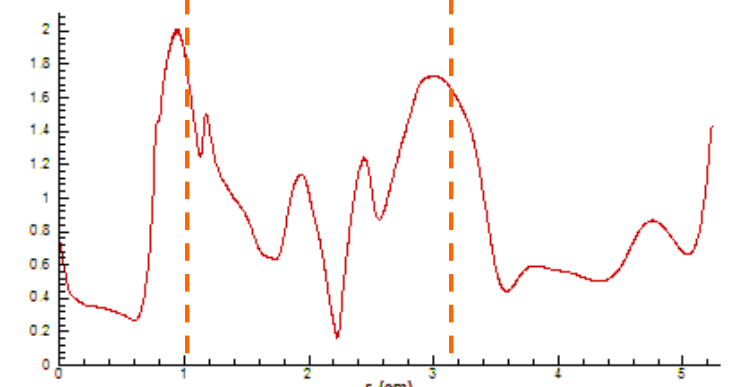
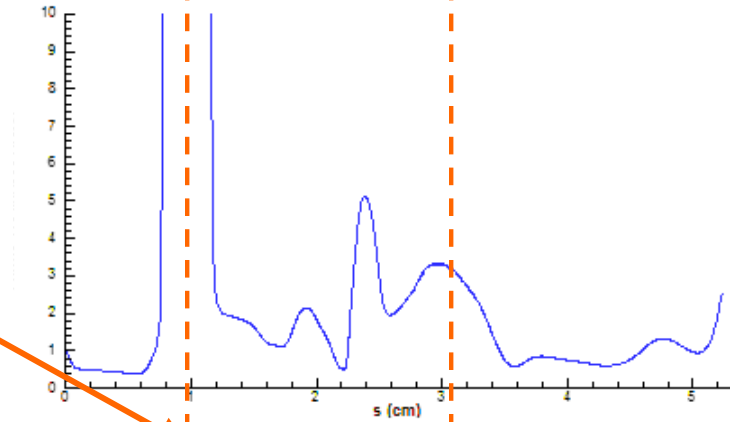
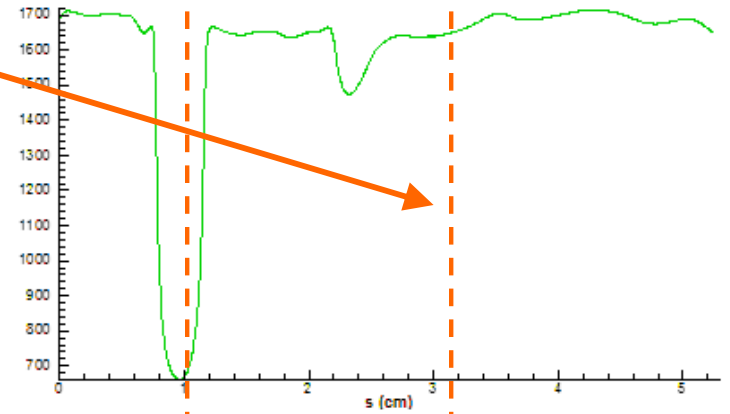
Flame weakens

Time = 2.85ms

T

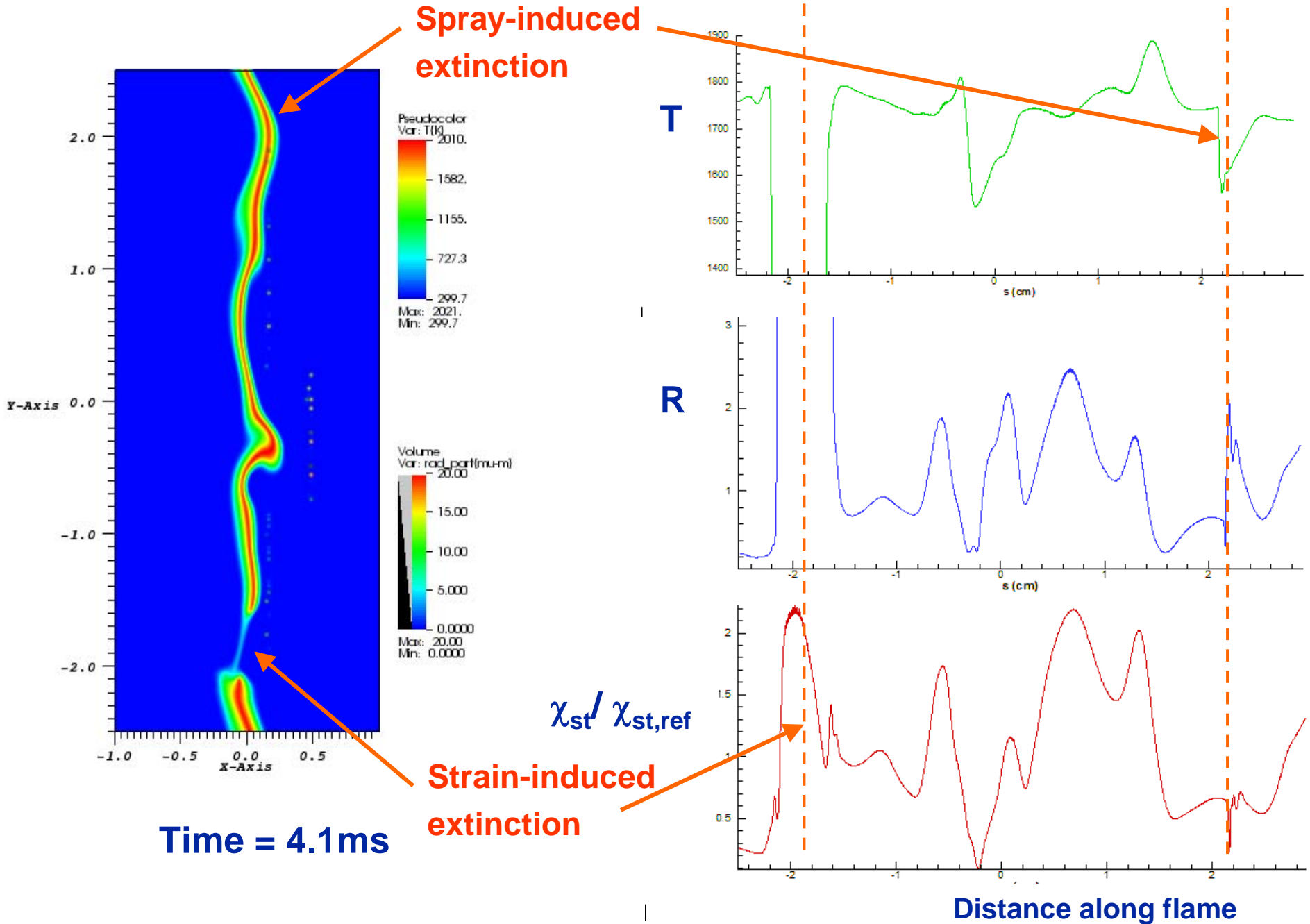
R

$\chi_{st} / \chi_{st,ref}$



Distance along flame

Turbulence with spray



Summary & Future Work



- ❑ **Modified extinction criterion was defined based on excess enthalpy variable.**
- ❑ **The criterion was extended for multi-component, detailed chemistry system by using the effective activation energy.**
- ❑ **Preliminary results suggested that the excess enthalpy variable properly accounts for the flame extinction caused by various flame weakening mechanisms.**
- ❑ **Additional parametric studies are needed to assess the effects of**
 - **Spray loading, size distribution, injection velocity**
 - **Strong transients**
 - **Differential diffusion**